

Hydrogen Fuel Cells

Modeling and Computations

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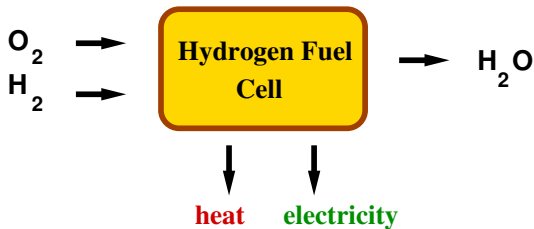
Outline

- 1 Introduction
- 2 Our modeling
 - Modeling the surface layer
 - The diffusion problem
- 3 Conclusion

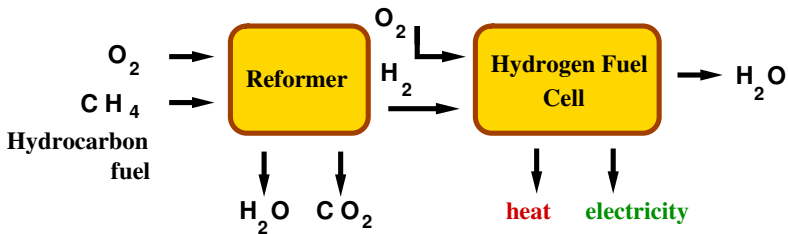
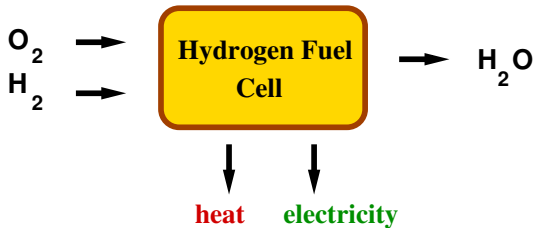
Overview of the talk

- The workings of a hydrogen fuel cell
- A mathematical model for hydrogen-palladium interaction
- Two mathematical problems:
 - Solution and analysis of an ODE
 - Solution and analysis of a PDE

Hydrogen fuel cells: overview



Hydrogen fuel cells: overview



Palladium: the element

palladium¹ (pə-lā'dē-əm) n.

Symbol **Pd**

1. A soft, ductile, steel-white, tarnish-resistant, metallic element occurring naturally with platinum, especially in gold, nickel, and copper ores. Because it can absorb large amounts of hydrogen, it is used as a purification filter for hydrogen and a catalyst in hydrogenation. It is alloyed for use in electric contacts, jewelry, nonmagnetic watch parts, and surgical instruments. Atomic number 46; atomic weight 106.4; melting point 1,552° C; boiling point 3,140° C; specific gravity 12.02 (20° C); valence 2, 3, 4. See note at **element**.

[From **Pallas** (discovered at the same time as the element)]

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Pallas (pāl'əs) n.

1. One of the largest asteroids, the second to be discovered.
2. *Greek Mythology* Athena.

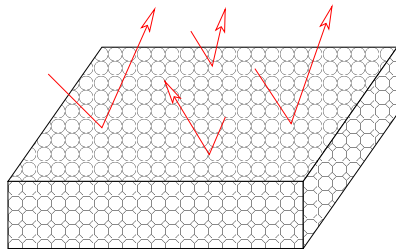
[After **Pallas** (Athena)]

The Hydrogen-Palladium interface

Γ_0 = rate of hydrogen molecules impacting a surface

Representative value: 10^{19} hits/cm²/sec

Γ_0 *proportional* to pressure



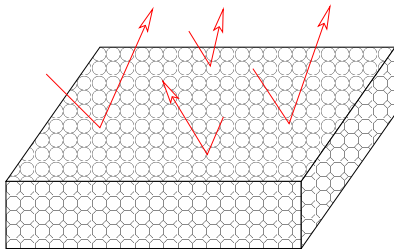
Around 10^{14} surface sites/cm²

The Hydrogen-Palladium interface

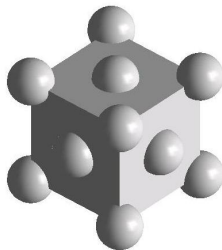
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Around 10^{14} surface sites/cm²



Modeling the surface layer

Fraction of occupied surface sites on the surface = α , $0 \leq \alpha \leq 1$

Rate of sticking = $\Gamma_0 S_0 (1 - \alpha)^2$, $S_0 \approx 0.3$

Rate of recombination = $k_d \alpha^2$

Equilibrium:

$$\Gamma_0 S_0 (1 - \alpha)^2 = k_d \alpha^2 \Rightarrow \left(\frac{1 - \alpha}{\alpha} \right)^2 = \frac{k_d}{\Gamma_0 S_0}$$

Fraction of occupied interior sites = β , $0 \leq \beta \leq 1$

Flow rate from surface to interior = $k_i \alpha (1 - \beta)$

Flow rate from interior to surface = $k_o \beta (1 - \alpha)$

Equilibrium:

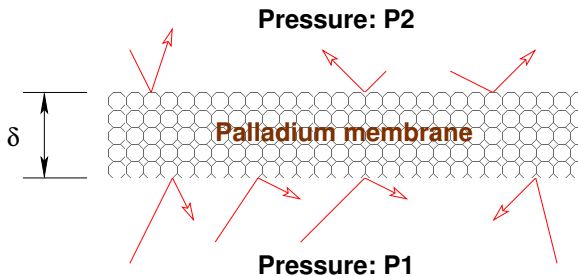
$$k_i \alpha (1 - \beta) = k_o \beta (1 - \alpha) \Rightarrow \frac{1 - \alpha}{\alpha} = \frac{k_o}{k_i} \frac{1 - \beta}{\beta}$$

Eliminate α :

$$\frac{\beta}{1 - \beta} = \frac{k_i}{k_o} \sqrt{\frac{\Gamma_0 S_0}{k_d}}$$

Diffusion through a membrane

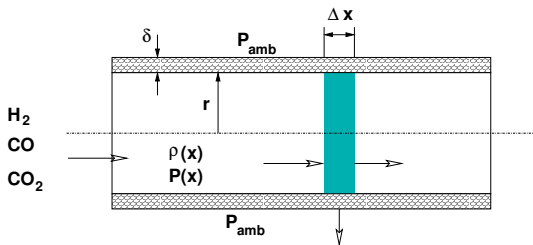
$$\beta \approx 0 \Rightarrow \beta = C_1 \sqrt{\Gamma_0} = C_2 \sqrt{P}$$



Concentrations near the surfaces: $C_2 \sqrt{P_1}$ and $C_2 \sqrt{P_2}$

$$\text{Flux} = \kappa \frac{\sqrt{P_1} - \sqrt{P_2}}{\delta}$$

Flow through a tube



$$\text{inflow} = \rho Av$$

$$\text{outflow} = (\rho + \Delta\rho)Av$$

$$\text{leakage} = (2\pi r \Delta x) \kappa \frac{\sqrt{P} - \sqrt{P_{\text{amb}}}}{\delta}$$

Conservation of mass

$$\rho Av = (\rho + \Delta\rho)Av + (2\pi r \Delta x) \kappa \frac{\sqrt{P} - \sqrt{P_{\text{amb}}}}{\delta}$$

Differential equation of pressure

Conservation of mass

$$\frac{d\rho}{dx} = -\frac{2\pi r\kappa}{Av\delta}(\sqrt{P} - \sqrt{P_{\text{amb}}})$$

Ideal Gas

$$P = RT\rho$$

$$\frac{dP}{dx} = -\frac{2\pi r\kappa RT}{Av\delta}(\sqrt{P} - \sqrt{P_{\text{amb}}})$$

Differential equation

$$\frac{dP}{dx} = -K(\sqrt{P} - \sqrt{P_{\text{amb}}}), \quad K = \frac{2\pi r\kappa RT}{F\delta}, \quad F = Av$$

Calculation of pressure

$$\frac{dP}{dx} = -K(\sqrt{P} - \sqrt{P_{\text{amb}}})$$

Calculation of pressure

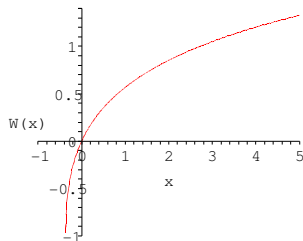
$$\frac{dP}{dx} = -K(\sqrt{P} - \sqrt{P_{\text{amb}}})$$

Solve for $P(x)$: $P(x) = P_{\text{amb}}[1 + W(z)]^2$

where $z = \frac{\sqrt{P(0)} - \sqrt{P_{\text{amb}}}}{\sqrt{P_{\text{amb}}}} \exp\left(\frac{\sqrt{P(0)} - \sqrt{P_{\text{amb}}} - \frac{1}{2}Kx}{\sqrt{P_{\text{amb}}}}\right)$

W : the *Lambert function*

$$ye^y = x \Leftrightarrow y = W(x)$$



Efficiency of hydrogen exchange

Rate of hydrogen inflow = $F\rho(0)$

Rate hydrogen outflow = $F\rho(L)$

Rate of hydrogen release: $F\rho(0) - F\rho(L)$

Efficiency:

$$\mathcal{E} = \frac{\text{rate of hydrogen release}}{\text{rate of hydrogen inflow}} = \frac{F\rho(0) - F\rho(L)}{F\rho(0)} = 1 - \frac{\rho(L)}{\rho(0)} = 1 - \frac{P(L)}{P(0)}$$

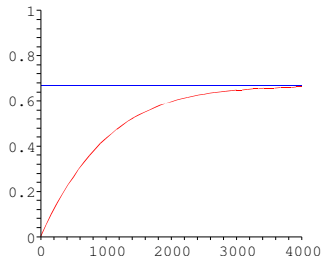
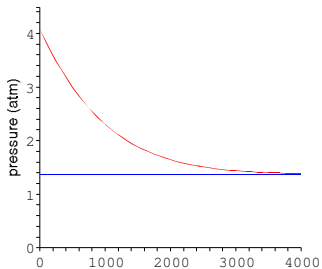
Best possible efficiency:

$$\mathcal{E}_{\max} = 1 - \frac{P_{\text{amb}}}{P(0)}$$

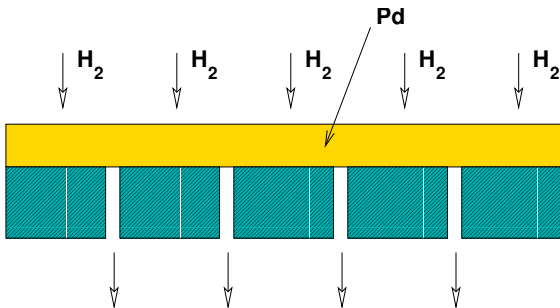
Numbers

tube radius	r	0.3175 cm
tube wall thickness	δ	0.0003 cm
flow rate	F	8330 cm ³ /sec
inlet pressure	$P(0)$	4.08 atm
ambient pressure	P_{amb}	1.36 atm
temperature	T	673 Kelvin
diffusivity	κ	6.96 10 ⁻⁸ mol/(cm sec atm ^{1/2})
gas constant	R	cm ³ atm / (mol Kelvin)

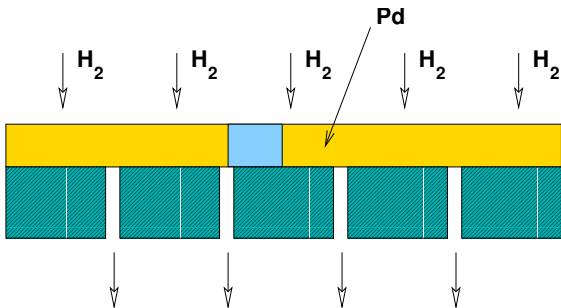
Results



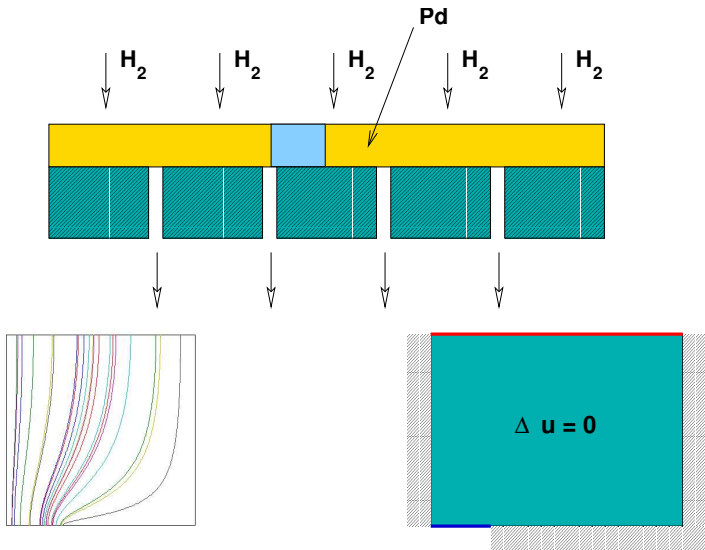
Membrane on porous support



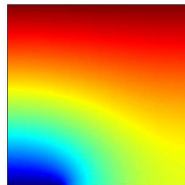
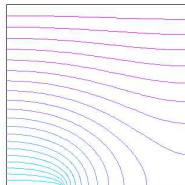
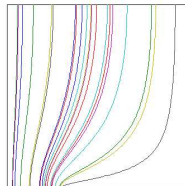
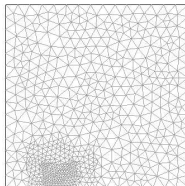
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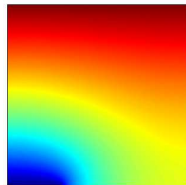
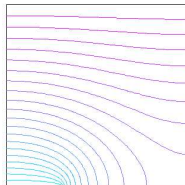
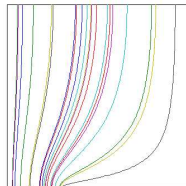
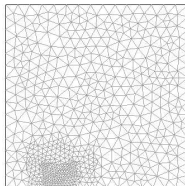
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Numerical solution with Femlab



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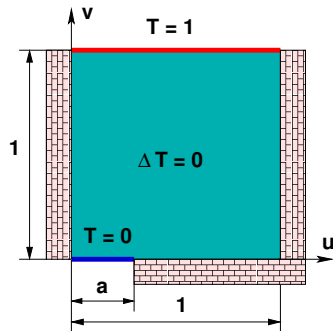


$$\int_0^1 \frac{\partial T}{\partial y}(x, 1) dx = 0.667$$

$$\int_0^{0.3} \frac{\partial T}{\partial y}(x, 0) dx = 0.627$$

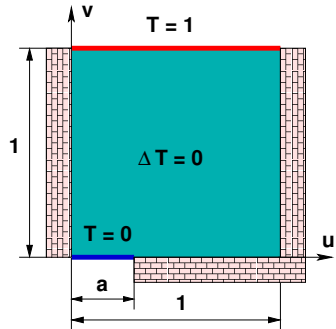
The limiting case

$$\text{Throughput} = J(a) = \int_0^a \frac{\partial T}{\partial v} \Big|_{v=0} du$$



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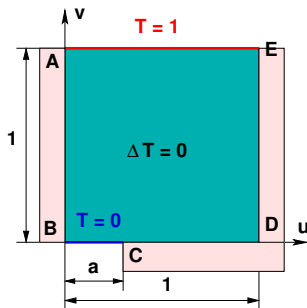
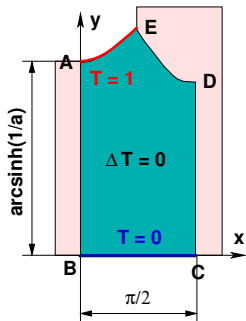


Theorem

Asymptotically, as $a \rightarrow 0$:

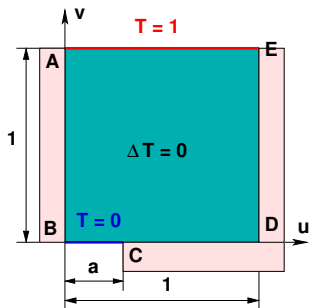
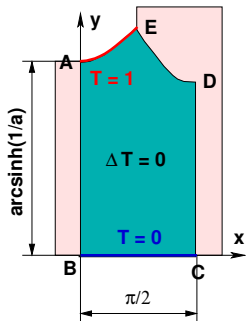
$$J(a) \approx \frac{\pi}{2 \ln \frac{2}{a}}.$$

Conformal mapping



$$u + iv = a \sin(x + iy) \Leftrightarrow u = a \sin x \cosh y, \quad v = a \cos x \sinh y$$

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$$T = T(x, y) \approx \frac{y}{\operatorname{arcsinh}(1/a)}$$

Proof of theorem

$$T(u, v) \approx \frac{1}{\operatorname{arcsinh} \frac{1}{a}} \operatorname{arccosh} \left[\frac{1}{2} \sqrt{\left(\frac{u}{a} + 1\right)^2 + \left(\frac{v}{a}\right)^2} + \frac{1}{2} \sqrt{\left(\frac{u}{a} - 1\right)^2 + \left(\frac{v}{a}\right)^2} \right]$$

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$$J(a) = \int_0^a \left. \frac{\partial T(u, v)}{\partial v} \right|_{v=0} du = ?$$

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$$J(a) = \int_0^a \left. \frac{\partial T(u, v)}{\partial v} \right|_{v=0} du = \frac{\pi}{2 \operatorname{arcsinh} \frac{1}{a}} \approx \frac{\pi}{2 \ln \frac{2}{a}} \quad QED$$

Thanks for your attention!!

Any question??

Acknowledgment

Fred Gornik, Power+Energy, Inc.

<http://powerandenergy.com>